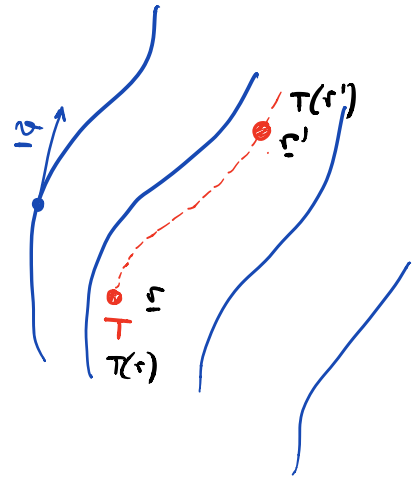


Equations of motion for a fluid

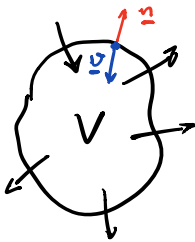
Material derivative

$$\frac{D}{Dt} = \underbrace{\frac{\partial}{\partial t}} + \underbrace{\underline{v} \cdot \nabla}$$

$$\frac{DT}{Dt} = \frac{\partial T}{\partial t} + \underline{v} \cdot \nabla T$$



Mass conservation



$$\frac{d}{dt} M_V = - \oint_{\partial V} \rho \underline{v} \cdot \underline{n} dS \quad \left. \begin{array}{l} \text{divergence} \\ \text{theorem} \end{array} \right\}$$

$$\hookrightarrow \frac{d}{dt} \int_V \rho dV = - \int_V \nabla \cdot (\rho \underline{v}) dV$$

$$\hookrightarrow \frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \underline{v}) = 0$$

$$\hookrightarrow \underbrace{\frac{\partial \rho}{\partial t}} + \rho (\nabla \cdot \underline{v}) + \underbrace{\underline{v} \cdot \nabla \rho} = 0$$

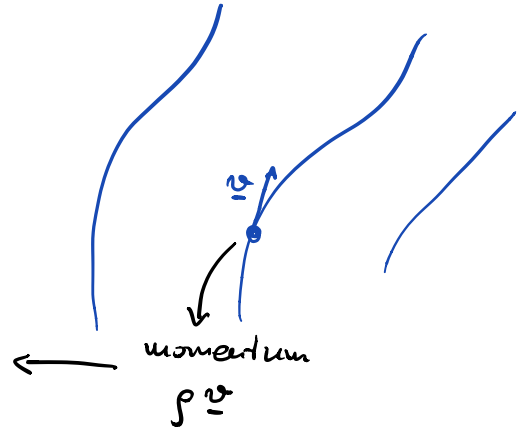
$$\hookrightarrow \underbrace{\frac{D\rho}{Dt}} = - \rho (\nabla \cdot \underline{v})$$

$\hookrightarrow$ incompressible fluid

$$\underbrace{\frac{D\rho}{Dt}} = 0 \quad \Rightarrow \quad (\nabla \cdot \underline{v}) = 0$$

Momentum conservation

- momentum advection
momentum gets carried
(along streamlines)

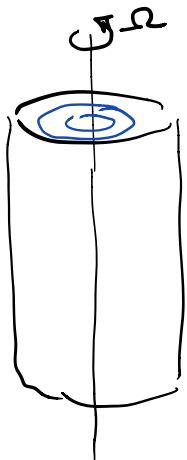


flux of
momentum

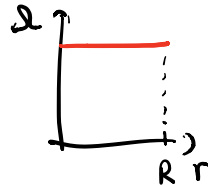
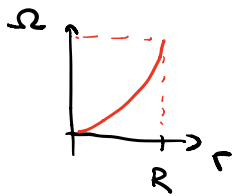
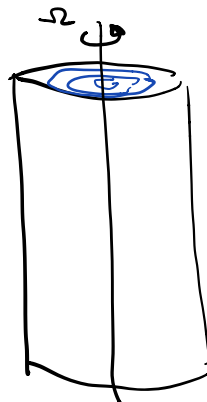
$$(\rho v) \cdot v$$

$$\sim \frac{\rho v^2}{2}$$

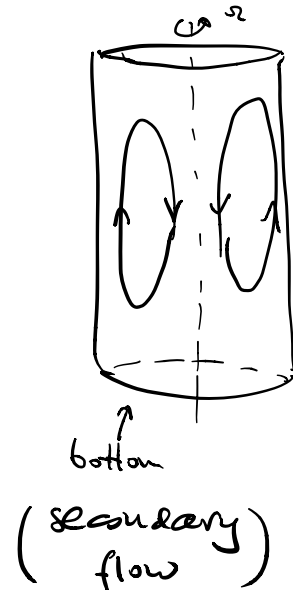
- Momentum diffusion



$t \rightarrow \infty$
 $\Rightarrow$



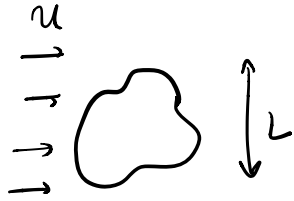
In the real world:



Navier - Stokes equation

$\underline{u}$, p , μ , ρ

$$\rho \frac{D\underline{u}}{Dt} = -\nabla p + \mu \nabla^2 \underline{u} = \rho \left[\frac{\partial \underline{u}}{\partial t} + (\underline{u} \cdot \nabla) \underline{u} \right]$$



Introduce dimensionless variables:

$$x^* = \frac{x}{L} \quad \underline{u}^* = \frac{\underline{u}}{u} \quad , \quad t^* = \frac{t}{T} \quad , \quad p^* = \frac{p}{\frac{\mu u}{L}}$$

$$\rho \left[\frac{u}{T} \frac{\partial \underline{u}^*}{\partial t^*} + \frac{u^2}{L} (\underline{u}^* \cdot \nabla^* \underline{u}^*) \right] = - \frac{\mu u}{L^2} \nabla^{*2} p^* + \frac{\mu u}{L^2} \nabla^{*2} \underline{u}^*$$

$$\underbrace{\frac{\rho L^2}{\mu T}}_{Re \cdot St} \frac{\partial \underline{u}^*}{\partial t^*} + \underbrace{\frac{\rho u L}{\mu}}_{Re} (\underline{u}^* \cdot \nabla^* \underline{u}^*) = - \nabla^{*2} p^* + \nabla^{*2} \underline{u}^*$$

$$Re = \frac{\rho u L}{\mu} \quad \text{Reynolds number}$$

$$St = \frac{L}{u T} \quad \text{Strouhal number}$$

$$Re \left[St \frac{\partial \underline{u}}{\partial t} + (\underline{u} \cdot \nabla \underline{u}) \right] = - \nabla^2 p + \nabla^2 \underline{u}$$

- (i) $St \ll 1$ quasi-steady limit $\rightarrow$ ok to ignore $\frac{\partial \underline{u}}{\partial t}$
- (ii) $St \gg 1$ rapidly changing flow $\rightarrow$ ok to ignore $\underline{u} \cdot \nabla \underline{u}$
- (iii) $Re \ll 1$ viscosity dominated $\rightarrow$ ok to ignore LHS
- (iv) $Re \gg 1$ inertially dominated $\rightarrow$ ok to ignore $\nabla^2 \underline{u}$ far from boundaries